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Experimental characterization and modelling of microfluidic radial diffusers for passive self-regulating valves

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Abstract

A microfluidic radial diffuser typically comprises a hole in a membrane facing a concentric pillar separated by a small gap where the fluid is forced to flow radially between the membrane and the pillar. Such diffusers are notably used to make passive flow rectification valves for drug delivery devices, wherein several holes are machined into a flexible membrane progressively deflecting against pillars as the pressure increases on top of it. The fluidic modelling of such a diffuser is made difficult by the presence of a transition region between the hole and the diffuser itself. An experimental investigation has been conducted using SOI wafers to form membranes having only one central hole and Pyrex wafers for the substrate and pillars. Both wafers are anodically bonded together after alignment. A simple fluidic model accounting for the specific geometry of the diffuser is proposed and compared to experimental results. A good match is obtained, for Reynolds number in the range 0.5 to 35, using the analytical formula of a radial diffuser in the laminar regime with an effective inner radius 40% smaller than the actual one, in order to correctly simulate the flow constriction at the entrance of the diffuser.

Keywords: Medical devices; Hydrodynamics; Laminar Flow; Microsystems; Micro Electro Mechanical Systems (MEMS); Micromanufacturing

1. Introduction

Passive flow rectification or flow control microvalves are microfluidic chips that can be used for cerebrospinal fluid management or drug delivery [1-2]. A typical application is an implantable pump for pain management. Such devices usually comprise a reservoir pressurized with liquefied gas and a flow restrictor. It is well known that these devices are sensitive to temperature variations. Flow rate variations up to +/- 13% per °C in body temperature change are reported [3]. Those systems will also deliver a different drug amount in environmental conditions of high pressures (scuba diving) or after a long exposition to high altitudes (up to +35% of over-delivery) [3]. Therefore, patients are advised to avoid these conditions. However, replacing the flow restrictor by a flow control valve makes the device insensitive to pressure variations. In addition, to limit under or overdoses, the implantable pump with a flow control valve offers the possibility to lower the reservoir pressure so as to limit risks during drug refilling process. Specific flow control valves may also comprise a passive compensation of the temperature effect on viscosity [4]. Microfluidic autoregulation obtained using the non-Newtonian rheological properties of polymeric solutions was reported by Groisman et al. [5, 6]. For the passive flow rectification of Newtonian fluids, different designs were reported, including 3D microfluidic devices made of stacks of PDMS layers [7-9], devices comprising spiral-shaped fluidic channels [10-12] or MEMS devices with micro-valves associated in parallel [1, 2, 4, 13].

Passive flow control can be achieved using a flexible silicon membrane having several through holes, each one being coupled with a concentric facing pillar etched in the substrate. The gap between the membrane and the top surface of the pillar depends on the reservoir pressure in direct communication with the top surface of the membrane. Increasing

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this pressure induces a change of the fluidic restriction hereafter referred to as “radial diffuser” or simply “diffuser” (see Fig. 1). This diffuser is significantly different from the typical conical diffuser valves described in the literature, which are mainly used for micropump applications [14-21]. The design of the device, including the determination of the number of hole/pillar pairs and their radial location along the membrane, may be achieved using a genetic algorithm as it is a powerful tool to get the configuration exhibiting the lowest sensitivity to machining tolerances [13]. A first fluidic model has been provided for devices with gap values (up to 30 μm) in the same order of magnitude as the membrane thickness itself. Flow control valves dedicated to the infusion of viscous drugs at high pressure lead to the use of very small gaps (typically 10 μm) and thick membranes (up to 130 μm). Such a specific geometry requires an improved fluidic model that better takes into account the abrupt change of flow direction as well as the very large flow constriction at the diffuser entrance. Microfluidic radial diffusers comprising a single hole at the center of the membrane and a single pillar have been produced and characterized. After a brief description of the process flow and the different designs investigated, the fluidic characterization of the samples is provided along with the new fluidic modelling of the radial diffuser.

Table 1 Notations

Symbol	Quantity
η	dynamic viscosity
ρ	fluid volumetric mass
R_h	hole radius
L_h	hole depth
R_p	pillar radius
h	Distance between the pillar and the membrane
d	valve off-centering
$\Delta P = P_{in} - P_{out}$	Pressure gradient
Q_i	flow rate via the fluidic pathway i
w_c	channel width
h_c	channel height
L_c	channel length
$R_{f\ out}$	fluidic resistance of the outlet
κ	correction parameter

2. Fluidic Model

2.1. Radial Diffuser

A schematic cross-section of the valve is shown in Fig. 1. The different notations in the text are given in Table I.

Flow control valve dedicated to high-pressure applications usually exhibits a small gap h :

$$h \ll R_h, R_p, L_h \dots \quad (1)$$

This specific geometry shall be analyzed further in order to model the different head losses.

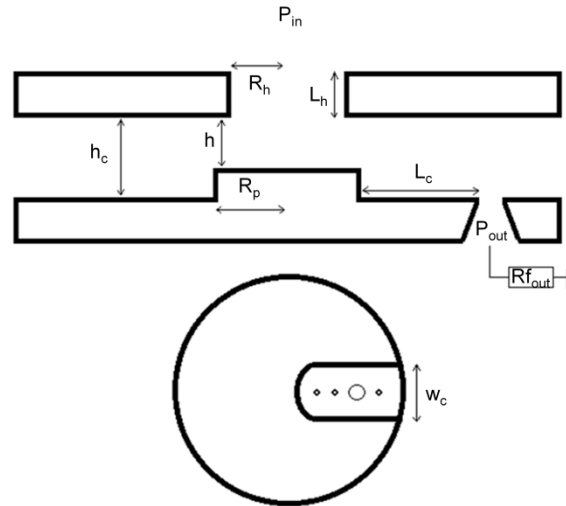


Figure 1 Schematic cross-section of a valve (top) and top view of the substrate having three pillars and one outlet hole inside a channel of width w_c (bottom)

The difference in pressure $\Delta P = P_{in} - P_{out}$ between the inlet and the outlet of the valve is written as a function of Q_i as follows:

$$\Delta P = \alpha_i Q_i^2 + \beta_i Q_i. \quad (2)$$

where i indicates one fluidic pathway, $\beta_i = \sum_i Rf_i$ is the sum of the fluidic resistances of the fluidic pathways i , and α_i is a function of the surfaces of each singularity. We estimate numerically the function $\alpha_i Q_i$ for each value of ΔP :

$$\alpha_i Q_i = -\frac{\beta_i}{2} + \sqrt{\alpha_i \Delta P + \frac{\beta_i^2}{4}}. \quad (3)$$

The total flow rate is, therefore:

$$Q = \sum_i Q_i. \quad (4)$$

We consider now a flow regulator that comprises several hole/pillar pairs.

2.2. Singular Head Losses

Fig. 2 (a) shows a schematic illustration of a radial diffuser, where the reservoir connected to the hole is at the pressure P , the cone represents the flow constriction before the diffuser itself and finally, the channel communicates with the outlet. The location of the different sources of singular head losses are noted, respectively: A for the contraction from the reservoir to the hole, B for the progressive contraction between the hole and the diffuser, C for the bend at the diffuser entrance, D for the radial expansion inside the diffuser and E for the vertical expansion from the diffuser to the channel. We define the cone opening angle γ as follows (see also Fig. 3):

$$\gamma = 2 \arctan \left(\frac{4\kappa R_{hi}}{L_h} \right). \quad (5)$$

Before entering into the diffuser, the flow experiences a bend with an angle equal to $\frac{\pi-\gamma}{2}$. According to [22], in the bend, the expression of the singular coefficient takes the form:

$$\sin^2 \left(\frac{\pi-\gamma}{4} \right) + 2 \sin^4 \left(\frac{\pi-\gamma}{4} \right). \quad (6)$$

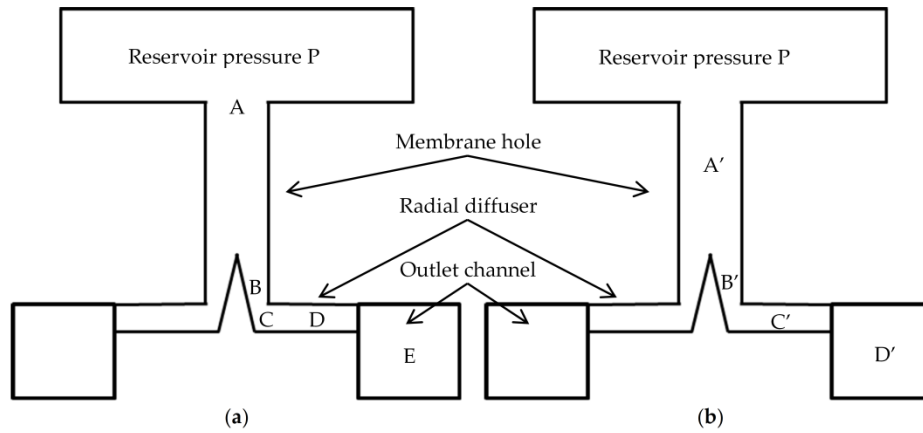


Figure 2 Schematic representations of the singular (a) and linear (b) head losses of a radial microfluidic diffuser. Each letter corresponds to a specific loss described in the text

For positive gradients of pressure, i.e. when the fluid flows through the hole, the diffuser, the fluidic channel and finally the outlet hole, the parameters α_i defined in (2) take the form (see [1] for the different expressions used):

$$\alpha_i = \frac{\rho}{2S^2} (A + B + C + D + E) = \frac{\rho}{2} \left(\frac{1}{\pi^2 R_{hi}^4} + \frac{0.4}{\pi^2} \left(\frac{1}{\kappa^2 R_{hi}^2 - (\kappa R_{hi} - h_i)^2} - \frac{1}{\kappa^2 R_{hi}^2} \right)^2 \left(1 - \frac{h_i}{\kappa R_{hi}} \right)^2 \sin(\gamma) + \frac{\sin^2(\frac{\pi-\gamma}{4}) + 2\sin^4(\frac{\pi-\gamma}{4})}{4\pi^2 \kappa^2 R_{hi}^2 h_i^2} + \frac{1}{4\pi^2 h_i^2} \left(\frac{1}{R_{pi}} - \frac{1}{\kappa R_{hi}} \right)^2 + \frac{\left(1 - \frac{h_i}{h_c} \right)^2}{4\pi^2 R_{pi}^2 h_i^2} \right). \quad (7)$$

where the terms A to E are the contributions of the fluidic elements shown in Fig. 2 (a).

The parameter κ has been introduced to better fit the experimental data when the gap is much smaller than the hole radius and the channel height, even at zero pressure. In that case, the parameter α_i can be simplified as follows:

$$\alpha_i = \frac{\rho}{2} \left(\frac{\sin^2(\frac{\pi-\gamma}{4}) + 2\sin^4(\frac{\pi-\gamma}{4}) + 0.4 \sin(\gamma)}{4\pi^2 \kappa^2 R_{hi}^2 h_i^2} + \frac{1}{4\pi^2 h_i^2} \left(\frac{1}{R_{pi}} - \frac{1}{\kappa R_{hi}} \right)^2 + \frac{1}{4\pi^2 R_{pi}^2 h_i^2} \right). \quad (8)$$

2.3. Linear Head Losses

The linear losses due to the fluid viscosity take place in four different locations as depicted in Fig. 2 (b): A' is the flow through the hole, B' is the flow constriction between the hole and the radial diffuser entrance (conical shape), C' is the flow through the radial diffuser, and D' is the flow in the outlet channel.

The parameters β_i defined in (2) take the form (see [1] for the different expressions used):

$$\beta_i = A' + B' + C' + D' = \frac{8\eta \left(\frac{3}{4} L_h + h_i \right)}{\pi R_{hi}^4} + \int_0^{\frac{L_h}{4}} \frac{8\eta}{\pi} \left(1 / \left(\kappa^4 R_{hi}^4 - b(x)^4 - \left(\frac{\kappa^2 R_{hi}^2 - b(x)^2}{\ln\left(\frac{\kappa R_{hi}}{b(x)}\right)} \right)^2 \right) \right) dx + \frac{6\eta}{\pi h_i^3} \ln\left(\frac{R_{pi}}{\kappa R_{hi}}\right) + \frac{12\eta L_{ci}}{w_{ci} h_{ci}^3}. \quad (9)$$

where the terms A' to D' are the contributions of the fluidic elements shown in Fig. 2 (b). Fig. 3 shows a schematic representation of the flow through the cone, which is an idealized representation of the transition between the hole and the diffuser entrance.

The parameter $b(x)$ used in the expression of the term B' takes the form:

$$b(x) = \begin{cases} \frac{4(\kappa R_{hi} - h_i)}{L_h} & \text{if } \kappa R_{hi} - h_i \geq 0 \\ 0 & \text{otherwise} \end{cases} \quad (10)$$

We also consider a fluidic resistance at the outlet Rf_{out} (due to the test setup or the connection to the patient for an infusion device). In that case, for a given pressure gradient ΔP , we estimate the flow rate Q as shown previously.

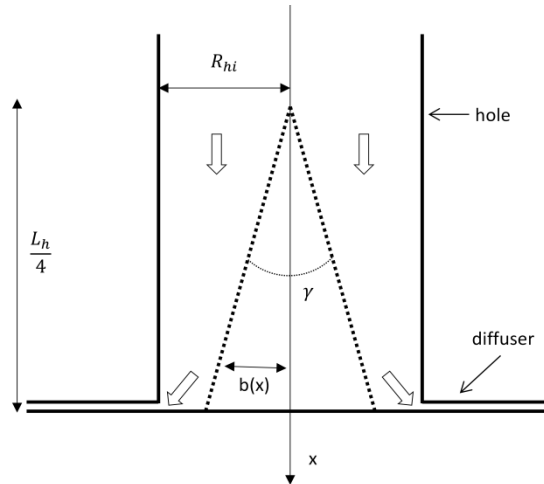


Figure 3 Schematic cross-section of the idealized flow transition between the hole and the diffuser entrance. The flow direction is indicated by arrows. The dashed line is an idealized representation of the transition between the hole and the diffuser entrance.

The additional pressure drop ΔP_{out} due to Rf_{out} is:

$$\Delta P_{out} = Rf_{out} Q. \quad (11)$$

And the effective gradient of pressure necessary to get the flow rate Q is, therefore:

$$\Delta P_{eff} = \Delta P + \Delta P_{out}. \quad (12)$$

3. Design and microfabrication

3.1. Design Description of the Prototypes

Specific designs of microfluidic radial diffusers have been made to better understand the fluidic behavior of such valves and to improve the fluidic modelling by adding a new parameter κ intended to be determined using experimental data. This parameter is a means to better simulate the flow constriction at the entrance of the diffuser, in particular, if the gap is small compared to other dimensions.

To prevent any error due to the estimation of the gap as the pressure increases, it has been decided to produce test devices having only one central hole/pillar pair. Up to the contact between the membrane and the substrate, the analytical formula giving the deflection as a function of the pressure p is valid as long as the deflection does not exceed $0.5t$, where t is the membrane thickness [23]:

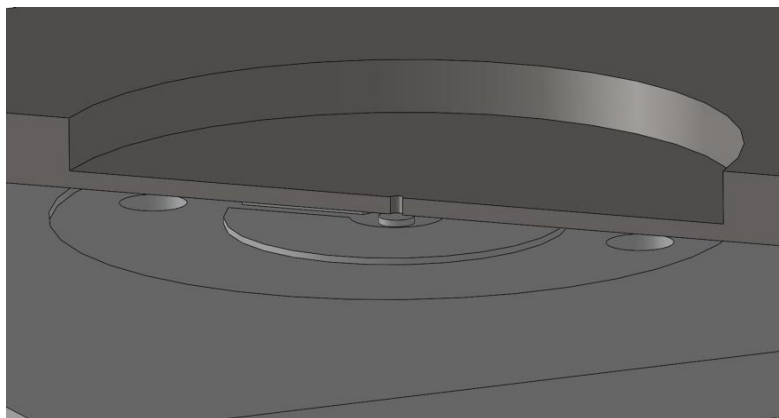
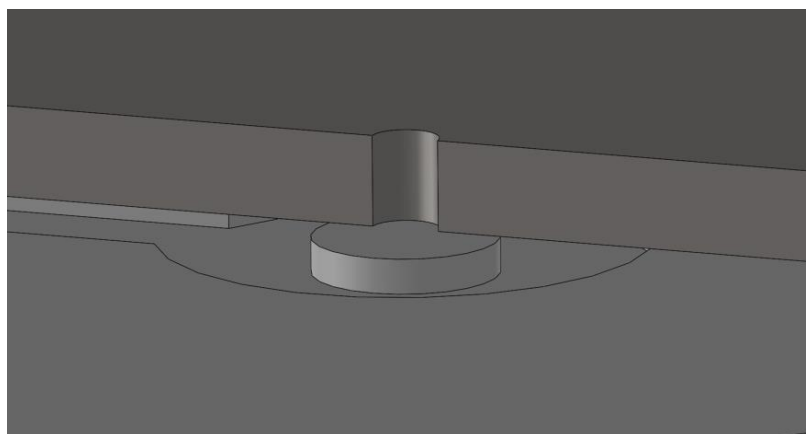
$$z_{max} = \frac{3 p R^4 (1 - \nu^2)}{16 E t^3}. \quad (13)$$

Where E is Young's modulus, ν is Poisson's ratio, and R is the membrane radius. The pillar height is fixed at $50 \mu\text{m}$ for all devices. The average measured dimensions of the samples are provided in Table II. The gap is measured with a mechanical profiler (Bruker Dektak XT surface profiler). The membrane thickness is obtained from the certificate of conformity of the SOI wafers, while the other dimensions are measured using an optical microscope Nikon Eclipse NV150 (software Kappa Metro). The ratio pillar radius/hole radius is in the range of 1.25 to 2.8.

Table 2 Key Dimensions of the Devices D1 to D7

Device #	Membrane thickness (μm)	Membrane radius (μm)	Gap (μm)	Hole radius (μm)	Pillar radius (μm)
D1	30	1879	10.4	48.4	138
D2	30	1580	10.2	48.4	137
D3	30	1428	10.3	48.3	137
D4	30	1329	10.4	48.4	136
D5	30	1257	10.3	48.3	137
D6	129.5	2560	10.3	48.4	132
D7	129.5	2560	10.8	61.5	77.5

A schematic cross-section of a device D6 is provided in Fig. 4a. The chip dimensions in mm are $10 \times 10 \times 1$ ($L \times W \times H$). The membrane (top wafer) contains one single inlet hole while the substrate has two outlet holes (to improve the priming of the device). A zoom of the radial diffuser at rest (membrane hole and pillar) is shown in Fig. 4b.

**Figure 4a** Schematic cross-section of the device D6 (membrane = top wafer, substrate = bottom wafer).**Figure 4b** Zoom of the radial diffuser D6

3.2. Manufacturing Process Flow

The holes and the membrane are made by dry etching (DRIE, Bosch process on Alcatel AMS200) of a 4" SOI wafers (front side and backside respectively). Two different SOI device layers have been considered: 30 μm and 129.5 μm . The buried oxide is 2 μm thick. Residues are removed with O_2 plasma and the final silicon oxide wet etching is obtained using a BHF 7:1 solution. The gap and pillars are obtained through isotropic wet etching (HF 10% at room temperature) of a 4" glass wafer (Borofloat 33, thickness 500 μm). The metallic hard mask used for the pillar definition was opened by dry etching (ion beam Veeco Nexus IBE350). The outlet hole (500 μm in diameter) in the glass substrate is made by sandblasting (IcoFlex Sarl, Ecublens, Switzerland). The two wafers are finally aligned at $\pm 10\mu\text{m}$ and anodically bonded together (Süss BA6/SB6). Chip singulation is performed using an automatic dicing saw Disco DAD321.

4. Fluidic characterization

The devices have been tested with filtered water at 20 °C. The water tank is pressurized by a pressure controller Druck DPI520 connected to high-pressure N_2 bottle (200 bar). A sample holder similar to the one described in [2] has been used for the tests. The flow rate is estimated by infusing at constant pressure during 1 minute into a beaker placed onto a scale Sartorius AC210P. The pressure ranges are 0 to 400 mbar for the devices D1 to D5 and 0 to 2.5 bar for the devices D6 and D7.

Typical flow rate versus pressure profiles measured using the thin (30 μm - devices D1 to D5) and thick (129.5 μm - devices D6 and D7) membranes are provided in Figures 5 and 6 respectively. Considering the different devices, the maximum Reynolds number varies within the range 0.5 to 35.

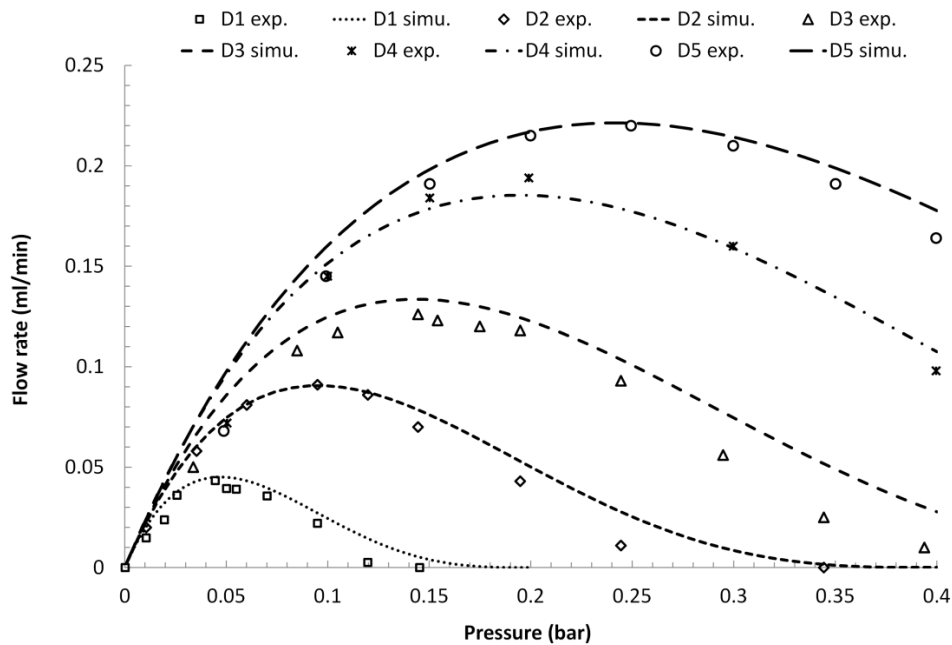


Figure 5 Flow rate versus pressure profiles of the devices D1 to D5 and comparison with numerical simulations using $\kappa = 0.6$

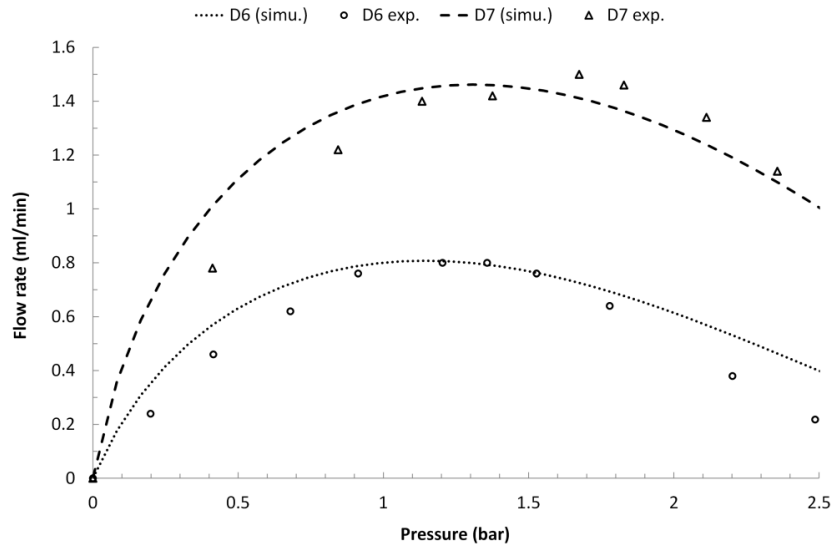


Figure 6 Flow rate versus pressure profiles of the devices D6 and D7 and comparison with numerical simulations using $\kappa = 0.6$

5. Results and discussion

The $Q(\Delta P)$ profiles shown in Figures 5 and 6 exhibit an asymmetric dome shape. By contrast to other radial valves wherein the fluidic behavior at low pressure is driven by the constant fluidic resistance of the membrane holes [1], we observe here that there is no linear regime even at low pressure. All tested devices exhibit a small value of the initial gap between the membrane and the pillar (about $10 \mu\text{m}$) and a large membrane hole diameter ($> 96 \mu\text{m}$). The fluidic resistance of the diffuser itself is therefore always dominant. Since the gap h decreases linearly with the applied pressure gradient ΔP (before contact), the fluidic resistance of this diffuser will increase as h (and therefore P) to the power -3 , preventing any linear regime in the fluidic characteristic of the devices.

Considering in a first and basic approximation that the flow resistance of the valve can be written:

$$R_f \approx \frac{a}{h^3} \quad (14)$$

Where a is a constant and h is the gap equal to the difference between the gap at rest h_0 and the deflection of the center of the membrane defined in Eq. (13):

$$h = h_0 - z_{max} = h_0 - u\Delta P \quad (15)$$

u is a constant that depends on the membrane characteristics (see Eq. (13)).

The flow rate in the valve can be approximated by a function having the following form:

$$Q = \frac{\Delta P}{R_f} \approx \frac{\Delta P}{a} (h_0 - u\Delta P)^3 \quad (16)$$

The devices D1 to D5 are similar except the membrane radius R , therefore the parameter u can be written:

$$u = cR^4 \quad (17)$$

Where c is a constant.

By replacing Eq. (17) in Eq. (16) we obtain:

$$Q \approx \frac{\Delta P}{a} (h_0 - cR^4\Delta P)^3 \quad (18)$$

The derivative of this function with respect to the pressure gradient is:

$$\frac{dQ}{d(\Delta P)} \approx \frac{(h_0 - 4cR^4 \Delta P)(h_0 - cR^4 \Delta P)^2}{a} \quad (19)$$

According to this approximation, the maximum flow rate is observed at a pressure gradient $\Delta P(Q_{max})$ which corresponds to the first root of this derivative:

$$\Delta P(Q_{max}) \approx \frac{h_0}{4cR^4} \quad (20)$$

The second root of this derivative corresponds to the pressure $\Delta P(Q_{vanish})$ at which the flowrate vanishes:

$$\Delta P(Q_{vanish}) \approx \frac{h_0}{cR^4} \quad (21)$$

Since both $\Delta P(Q_{van})$ and $\Delta P(Q_{max})$ are proportional to the membrane radius R at the power -4 , the larger the value of the membrane radius the smaller the value of the pressure at which the flow rate vanishes and the value of the pressure at the top of the dome as observed experimentally.

The introduction of $\Delta P(Q_{max})$ (see Eq. 20) in the equation (18) leads to a value of Q_{max} that is also proportional to $1/R^4$:

$$Q_{max} \approx \frac{27h_0^4}{256acR^4} \quad (22)$$

The simplified model introduced at the beginning of this section is, therefore, useful to explain the trend of the experimental curves, including the fact that the bigger membranes have the smallest flow rates, in good agreement with the experimental observations (see Figure 5).

However, in order to fit the experimental data, the whole expressions of the singular and linear head losses shall be used. The average measured misalignment of 10 μm between the pillars and the membrane holes has also been introduced into the model. The gap varies in principle between h_0 (at rest) and 0 (at high pressure, when the membrane is in contact with the pillar). Since we use a particle filter that exhibits a pore size of 0.2 μm , we fix the minimum gap to 0.2 instead of 0 μm , assuming that contamination could prevent the total closure of the valve.

As mentioned in the introduction, the original fluidic modelling (see [1]) is not adapted to a radial diffuser that exhibits a gap that is much smaller than all other dimensions of the devices. A parameter κ has therefore been introduced into the model as shown in section II, to better account for the flow constriction at the diffuser entrance. The data analysis has been carried out focusing on the central part of the curves, for pressure values centered around $\Delta P(Q_{max})$, since the measurement errors are smaller at high flowrate. Moreover, a flow control valve usually includes several radial diffusers, and the behavior of the valve is mainly secured by the radial diffuser that is located near the outer edge of the membrane. The flow rate through this diffuser remains large at high pressure while all other radial diffusers located nearer to the center of the membrane are almost closed (these other radial diffusers are only used to fine-tune the flow profile at low pressure). Therefore the overall fluidic characteristic of the valve is driven by the high flow parts of the different radial diffusers (the diffusers located near the membrane centre at low pressure and the outer diffuser at high pressure). Considering this limitation, a good match between experiment and simulation (in Matlab) is obtained using $\kappa = 0.6$. It should be noted that the use of a single parameter is not sufficient to perfectly fit the tail of the different curves at high pressure.

5.1. Application to the characterization of the non-linear deformation of a membrane against a rigid substrate

As mentioned in [23], the highly non-linear deflection of a clamped membrane against a rigid substrate has no simple analytical solution. FEM simulations can be carried out to determine, at different test pressures, the gap between the membrane and the substrate as a function of the radial position, but the experimental validation of the modelling is relatively complex, in particular at high pressure. To improve the reliability of the gap estimation as a function of the applied pressure, it is proposed to perform the fluidic characterization of chips that exhibit the same radial diffusers located at different radial positions.

We first assume that the correction due to the membrane tilt is small (membrane diameter \gg gap) [2].

Description of the “fluidic” method to derive the non-linear deformation of the membrane:

A fluidic model for the valve is established by measuring the flow rate versus pressure characteristic of the chip with the centered diffuser: the evolution of the fluidic resistance of the valve as a function of the gap $R_f(gap)$ is derived since the deflection of the center of a clamped membrane is well known [23].

The fluidic resistance of the same (i.e. same geometry) but off-centered diffuser is measured: for this given radial position of the diffuser the function $R_f(pressure)$ is derived.

With each value of the fluidic resistance is associated a value of the gap using the interpolation of the function $R_f(gap)$: the function $gap(pressure)$ is therefore derived for a given value of the nominal gap and for a given membrane (material, diameter, and thickness).

This method was applied to the diffuser design D6 (see Table II for the diffuser design). A similar diffuser had previously been used in a flow control valve (see reference [2], design A, with a nominal flow rate of 0.5 mL/min at 12 cP). There is however a small discrepancy regarding the pillar diameter (-15%) due to over-etch during the processing of the samples D6.

Samples were made according to the process flow described in §3. We consider a diffuser design D6 located at a distance of 2.09 mm from the membrane center. The diffuser was characterized by the test setup described in reference [2] up to 18 bar. The value of the “fluidic” gap versus the fluidic resistance was derived using the data provided in Figure 6. Finally, the interpolated value of the “fluidic” gap between the membrane and the pillar at the radial position 2.09 mm was derived using this “fluidic” probe (see Figure 7). Such an indirect estimation of the membrane deflection (“fluidic probe”) could be a simple alternative to the development of a specific and complex characterization setup at high pressure. This method is indeed a bypass to the direct measurement of the real gap: the function $gap(pressure)$ can be introduced into the fluidic model described in section 2. By definition, the model is able to reproduce the experimental data obtained during the fluidic test of this specific diffuser, but errors due to interpolation and to the approximation made in the fluidic model are expected if the diffuser dimensions and/or radial position are modified. If the nominal value of the gap is small compared to all other dimensions, its value is usually the critical-to-quality parameter that shall be controlled in fabrication. Moreover, to determine the ideal value of the diffuser gap, it is recommended to investigate experimentally the effect of small variations of this parameter onto the fluidic characteristic of the microfluidic chips having such radial diffusers (the initial nominal gap value being derived from simulations). This method is of course only relevant in case of highly non-linear deformation of the membrane.

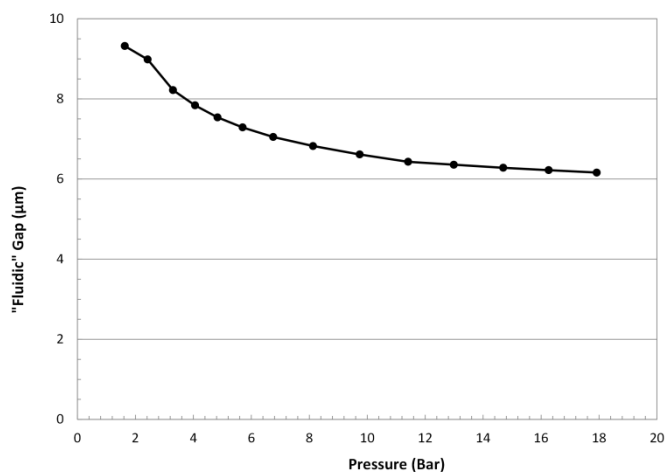


Figure 7 Interpolated value of the “fluidic” gap between the membrane and the pillar at the radial position 2.09 mm as a function of the applied pressure for a diffuser design D6 (see Table II).

6. Conclusion

The numerical modelling of a microfluidic radial diffuser formed of a gap, much smaller than other critical dimensions, between a membrane and a pillar has been investigated. We observe, based on the analysis of the experimental data provided in Figs. 5 and 6, that the linear losses at the interconnection between the hole and the diffuser are simulated considering an increase of the constriction length of the diffuser. A single parameter κ has been used to adjust the model accordingly to the experimental data. The expressions of the singular losses account for the specific geometry of the problem (especially the bend at the diffuser's entry and the diffuser itself). A match between modelling and experiments better than 15% for a Reynolds number varying from 0.5 to 35 and a ratio pillar radius/hole radius in the range of 1.25 to 2.8 has been obtained. At very high pressure, when the valve is almost closed, additional corrections to the model are necessary to simulate the radial diffuser which becomes really sensitive to particulate contamination and surface roughness. The association of several microfluidic diffusers inside a single membrane will allow to obtain a constant flow rate over a predefined range of pressure. This analytical model of the radial diffuser is useful to design a microfluidic chip without complex 3D FEM simulations and metrology tools.

Compliance with ethical standards

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Disclosure of conflict of interest

The authors declare no conflict of interest.

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